solvent; and

(c) crystallizing a phytosterol product, wherein the phytosterol product is substantially citrostadienol-free.--

--10. (New) The process according to claim 9, wherein the distillation residue comprises a deodorizer condensate obtained from fatty acid methyl ester production.--

--11. (New) The process according to claim 10, wherein the deodorizer condensate is derived from an oil selected from the group consisting of rapeseed oil and sunflower oil.--

--12. (New) The process according to claim 11, wherein the oil comprises sunflower oil.--

--13. (New) The process according to claim 9, wherein the distillation residue comprises tall oil pitch.--

--14. (New) The process according to claim 9, wherein the alkanol comprises methanol.--

--15. (New) The process according to claim 11, wherein the alkanol comprises methanol.--

--16. (New) The process according to claim 9, wherein the liquid phytosterol starting material is maintained at a temperature of from 60°C to 80°C prior to and during dissolution in the hydrocarbon solvent.--

--17. (New) The process according to claim 11, wherein the liquid phytosterol starting material is maintained at a temperature of from 60°C to 80°C prior to and during

dissolution in the hydrocarbon solvent.--

--18. (New) The process according to claim 16, wherein the liquid phytosterol starting material is maintained at a temperature of from 65°C to 70°C.--

--19. (New) The process according to claim 17, wherein the liquid phytosterol starting material is maintained at a temperature of from 65°C to 70°C.--

--20. (New) The process according to claim 9, wherein the hydrocarbon solvent comprises a linear or branched alkane isomer selected from the group consisting of pentane, hexane, heptane, octane, nonane, decane, and mixtures thereof.--

--21. (New) The process according to claim 9, wherein the hydrocarbon solvent comprises a linear or branched alkane isomer selected from the group consisting of hexane, heptane, and mixtures thereof.--

--22. (New) The process according to claim 9, wherein methanol is combined with the hydrocarbon solvent prior to crystallization.--

--23. (New) The process according to claim 22, wherein the methanol is present in an amount of from 1 to 15 % by weight, based on the hydrocarbon solvent.--

--24. (New) The process according to claim 11, wherein methanol is combined with the hydrocarbon solvent prior to crystallization.--

--25. (New) The process according to claim 24, wherein the methanol is present in an amount of from 1 to 15 % by weight, based on the hydrocarbon solvent.--

--26. (New) The process according to claim 16, wherein methanol is

combined with the hydrocarbon solvent prior to crystallization.--

--27. (New) The process according to claim 26, wherein the methanol is present in an amount of from 1 to 15 % by weight, based on the hydrocarbon solvent.--

--28. (New) The process according to claim 9, wherein crystallizing the phytosterol product comprises cooling the liquid phytosterol starting material in the hydrocarbon solvent to a temperature of below about 30°C.--

--29. (New) The process according to claim 9, wherein crystallizing the phytosterol product comprises cooling the liquid phytosterol starting material in the hydrocarbon solvent to a temperature of from about 25°C to about 30°C.--

--30. (New) The process according to claim 11, wherein crystallizing the phytosterol product comprises cooling the liquid phytosterol starting material in the hydrocarbon solvent to a temperature of below about 30°C.--

--31. (New) The process according to claim 11, wherein crystallizing the phytosterol product comprises cooling the liquid phytosterol starting material in the hydrocarbon solvent to a temperature of from about 25°C to about 30°C.--

--32. (New) The process according to claim 9, wherein the phytosterol product has a citrostadienol content of less than 0.5% by weight.--

--33. (New) The process according to claim 9, wherein the phytosterol product has a citrostadienol content of less than 0.2% by weight.--

--34. (New) A process for preparing phytosterols, said process comprising:

(a) providing a liquid phytosterol starting material obtained by

transesterification of a distillation residue with methanol, wherein the distillation residue comprises a deodorizer condensate derived from sunflower oil;

(b) dissolving the liquid phytosterol starting material in a hydrocarbon solvent, the hydrocarbon solvent comprising a linear or branched alkane isomer selected from the group consisting of hexane, heptane, and mixtures thereof, wherein the liquid phytosterol starting material is maintained at a temperature of from 60°C to 80°C prior to and during dissolution in the hydrocarbon solvent; and

(c) crystallizing a phytosterol product via cooling the liquid phytosterol starting material in the hydrocarbon solvent to a temperature of below about 30°C, wherein methanol is combined with the hydrocarbon solvent prior to crystallization in an amount of from 1 to 15 % by weight, based on the hydrocarbon solvent, and wherein the phytosterol product has a citrostadienol content of less than 0.5% by weight.--

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--35. (New) A phytosterol prepared by the process according to claim 1.--

--36. (New) A phytosterol prepared by the process according to claim 34.--

--37. (New) A composition comprising one or more natural phytosterol compounds, wherein the composition has a citrostadienol content of 0.5% by weight or less.--

Please cancel claims 1-8, without prejudice.